

AMENDMENTS TO THE CLAIMS:

This listing of claims will replace all prior versions, and listings, of claims in the application:

1 (previously presented). A process for the oxidation of a C₂ to C₄ alkane to produce the corresponding alkene and carboxylic acid which process comprises:

contacting in an oxidation reaction zone, said alkane, molecular oxygen-containing gas and the corresponding alkene in the presence of at least one catalyst active for the oxidation of the alkane to the corresponding alkene and carboxylic acid, to produce a product stream comprising alkene, carboxylic acid and water; and

adjusting or maintaining the molar ratio of alkene produced in said oxidation reaction zone to carboxylic acid produced in said oxidation reaction zone by controlling the concentration of the alkene introduced in said oxidation reaction zone.

2 (previously presented). An integrated process for the production of an alkyl carboxylate which process comprises the steps:

(a) contacting in an oxidation reaction zone a C₂ to C₄ alkane, a molecular oxygen-containing gas and the corresponding alkene in the presence of at least one catalyst active for the oxidation of the alkane to the corresponding alkene and carboxylic acid, to produce a product stream comprising alkene and carboxylic acid and water; adjusting or maintaining the molar ratio of alkene produced in said oxidation reaction zone to carboxylic acid produced in said oxidation reaction zone by controlling the concentration of alkene introduced in said oxidation reaction zone; and

(b) contacting in a second reaction zone at least a portion of each of said alkene and carboxylic acid produced in the first reaction zone, in the presence of at least one catalyst active for the production of alkyl carboxylate to produce said alkyl carboxylate.

3 (previously presented). An integrated process for the production of an alkenyl carboxylate which process comprises the steps:

(a) contacting in an oxidation reaction zone a C₂ to C₄ alkane, a molecular oxygen-containing gas, and the corresponding alkene and optionally, water in the presence of at least one catalyst active for the oxidation of the alkane to the corresponding alkene and carboxylic acid, to produce a product stream comprising alkene and carboxylic acid and water; adjusting or maintaining the molar ratio of alkene produced in said reaction zone to carboxylic acid produced in said oxidation reaction zone by controlling the concentration of alkene introduced in said oxidation reaction zone; and

(b) contacting in a second reaction zone at least a portion of each of said alkene and carboxylic acid produced in the first reaction zone and a molecular oxygen-containing gas, in the presence of at least one catalyst active for the production of alkenyl carboxylate to produce said alkenyl carboxylate.

4 (previously presented). A process as claimed in claim 1, 2 or 3 in which the molar ratio of alkene to carboxylic acid produced in the oxidation reaction zone is in the range 10:1 to 1:10.

5 (previously presented). A process as claimed in claim 1, 2 or 3 in which the molar ratio of alkene to carboxylic acid produced in the oxidation reaction zone is in the range 0.8 : 1 to 1.4 : 1.

6 (previously presented). A process as claimed in claim 2 or claim 3 in which alkene and/or carboxylic acid is separately recovered from the oxidation reaction product or separately added to the second reaction zone.

7 (previously presented). A process as claimed in claim 1, 2 or 3 in which the alkane is ethane, the corresponding alkene being ethylene and the corresponding carboxylic acid being acetic acid.

8 (previously presented). A process according to claim 2 wherein the alkyl carboxylate is ethyl acetate.

9 (previously presented). A process according to claim 3 wherein the alkenyl carboxylate is vinyl acetate.

10 (previously presented). A process according to claim 8 or claim 9 and wherein the molar ratio of alkene to carboxylic acid produced in the oxidation reaction zone is in the range 0.8: 1 to 1.4:1.

11 (previously presented). A process according to claim 1, 2 or 3 wherein the concentration of alkene fed to the oxidation reaction zone is from greater than 0 and up to and including 50 mol% of the total feed, including recycles.

12 (previously presented). A process according to claim 1, 2 or 3 wherein the concentration of water fed to the oxidation reaction zone is from 0 to 50 mol% inclusive of the total feed, including recycles.

13 (previously presented). A process according to claim 1, 2 or 3 wherein alkene and water are fed into the oxidation reaction zone.

14 (previously presented). A process according to claim 1, 2 or 3 wherein the alkene and water are fed into the oxidation reaction zone in an alkene : water ratio of 1 to 0.1-250 by weight.

15 (original). A process according to claim 14 wherein the ratio of alkene : water is 1 to 0.1-10 by weight.

16 (original). A process according to claim 15 wherein the molar ratio of alkene : carboxylic acid is in the range 0.8: 1 to 1.4 : 1.

17 (previously presented). A process according to claim 1, 2 or 3 in which the at least one catalyst in the oxidation reaction zone comprises molybdenum.

18 (original). A process according to claim 3 in which the at least one catalyst in the second reaction zone comprises palladium.

19 (previously presented). A process according to claim 1, 2 or 3 in which the oxidation reaction is carried out at a temperature in the range 100 to 400 °C.

20 (previously presented). A process according to claim 1, 2 or 3 in which the oxidation reaction is carried out at atmospheric or superatmospheric pressure.

21 (previously presented). A process according to claim 1, 2 or 3 in which the oxidation reaction is carried out at a GHSV of 500-10,000 hr⁻¹.

22 (previously presented). A process according to claim 1, 2 or 3 wherein the product stream from the oxidation reaction zone also comprises carbon oxides in an amount of less than 15 mol%.

23 (previously presented). A process according to claim 1, 2 or 3 in which the alkane is ethane, the corresponding alkene is ethylene, the corresponding carboxylic acid is acetic acid and wherein ethylene and water are fed into the oxidation reaction zone in a ratio of 1 to 0.1-10 by weight, the molar ratio of ethylene to acetic acid produced is in the range 0.8: 1 to 1.4 : 1 and the product stream from the oxidation reaction zone also comprises carbon oxides in an amount of less than 15 mol%.

24 (previously presented). A process according to claim 1, 2 or 3, wherein water is introduced into the oxidation reaction zone.

25 (previously presented). A process according to claim 1, 2 or 3, wherein said adjusting or maintaining step is performed by controlling one or more of the pressure, temperature and residence time of the oxidation reaction zone.

26 (previously presented). A process according to claim 1, 2 or 3, wherein said contacting step is carried out in the presence of water and wherein said adjusting or maintaining step is performed by controlling one or more of the pressure, temperature and residence time of the oxidation reaction zone.